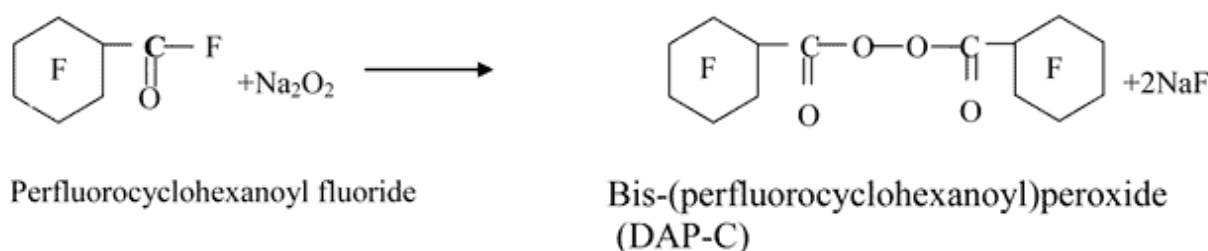


1. RC316 (1,2-dichlorohexafluorocyclobutane), the most close analogue of CFC113, that results from the cyclo-dimerisation of trifluorochloroethylene as a mixture of a few isomers. Due to exhaustive halogenation of RC316 its inertness in radical polymerisation is comparative to that of CFC113. RC316 is non-combustible and non-explosive. The substance is ozone-depleting, but yet non-regulated by the Montreal Protocol. Its price is comparable to that of CFC113.
2. MD46 (perfluoromethyldiethylamine) is a by-product in perfluorotriethylamine production. It is the less-common of the solvents under consideration. The substance is highly resistant to radical processes, and enables to achieve the best strength and proton conductivity. The estimated price is given below.
3. PSVE. The method of co-polymerisation using the ether monomer PSVE for solvent is also mentioned in literature [1, 2]. However, with this method it is very difficult to provide constant composition of the copolymer product; and the monomer losses during its regeneration increase. The main properties of considered solvents are shown below in Table 1.

Table 1. Characteristics of solvents for solution polymerisation.

Solvent	Chemical formula	Resistance to radicals	MAC, mg/m ³	Boiling temperature, oC	Availability	Price, ruble/kg
RC316	C ₄ F ₆ Cl ₂	Middle	10	59	Low	2000
MD46	C ₅ F ₁₃ N	High	500	46	Low	9000
PSVE	C ₇ F ₁₄ O ₄ S	–	50	-6	middle	20000

The solvent impact on the destruction of the co-polymerisation initiator was studied. Bis-(perfluorocyclohexanoyl)peroxide (DAP-C) was used for initiator; the substance synthesis is based on the interaction between perfluorocyclohexane carbonyl fluoride (PFCHC) and Na₂O₂, formed by the reaction between NaOH and hydrogen peroxide.



Thermal decomposition of DAP-C in a solvent under study was conducted in a sealed glass sample-tube placed into an ultra-thermostat. The temperature was being kept constant with accuracy 0.1B°C. The peroxide concentration was determined by iodometric titration in equal time intervals. A graph of peroxide concentration dependence on its decay-period was constructed, and, hence, the peroxide half-decay period was determined. The results are shown in Table 2.

Table 2. DAP-C thermal decomposition in various solvents.

Solvent	DAP-C half-decay period		
	30B°C	40B°C	50B°C
CFC113	~49 hour	13 hour 45 min	3 hour 47 min
MD-46	~41 hour	10 hour 15 min	2 hour 30 min

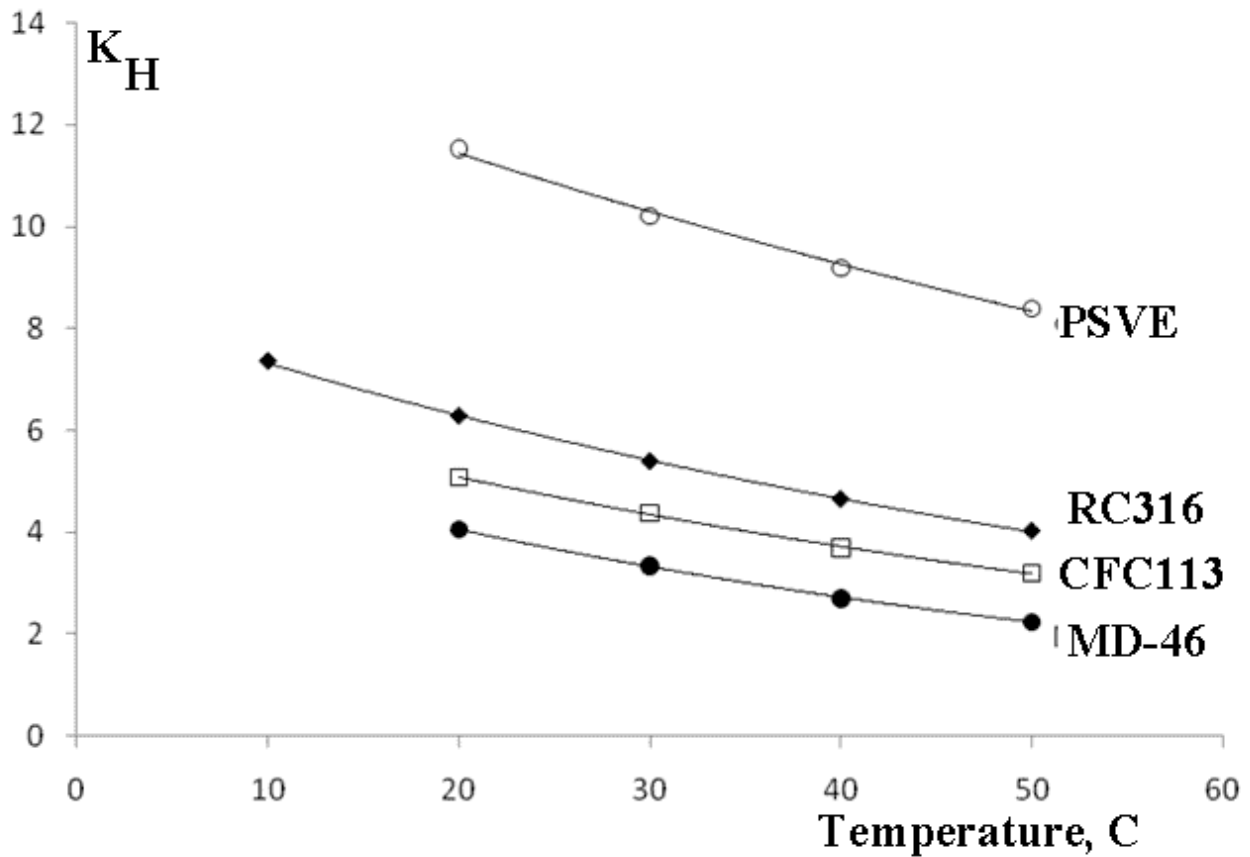
RC316	~44 hour	11 hour 40 min	3 hour 05 min
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From Table 1 one may see that DAP-C half-decay periods in MD-46 and RC316 are very close, and consequently, from this point of view, both solvents may be considered as acceptable CFC113 substituents.

TFE solubility in PSVE and in solvents was studied within the working temperature interval.

TFE solubility was studied in a 0.2 dm³ reactor equipped with a stirrer, jacket, thermocouple (accuracy 0.1B°C), and manometer (accuracy 0.1atm). 150g of the solvent under study was charged into the preliminary evacuated reactor at room temperature, and TFE was fed to total pressure 2 atm. Then we started raising the reactor temperature by step of 10B°C; at each step the procedure stopped for 1 hour to achieve equilibrium, and recorded both temperature and pressure values. TFE gas-phase concentration was calculated from the reactor pressure and reference density values. Our calculations took into account the solvent specific vapour pressure and its amount turned into gas phase. TFE liquid-phase concentration was determined by subtraction of gas-phase TFE amount from that charged into the reactor.

The solvent Henry constants are graphically shown in Figure 1.



K_H - Henry constant, TFE concentration in liquid : TFE concentration in gas phase.

Figure 1. TFE solubility in PSVE, RC316, MD46, and CFC113.

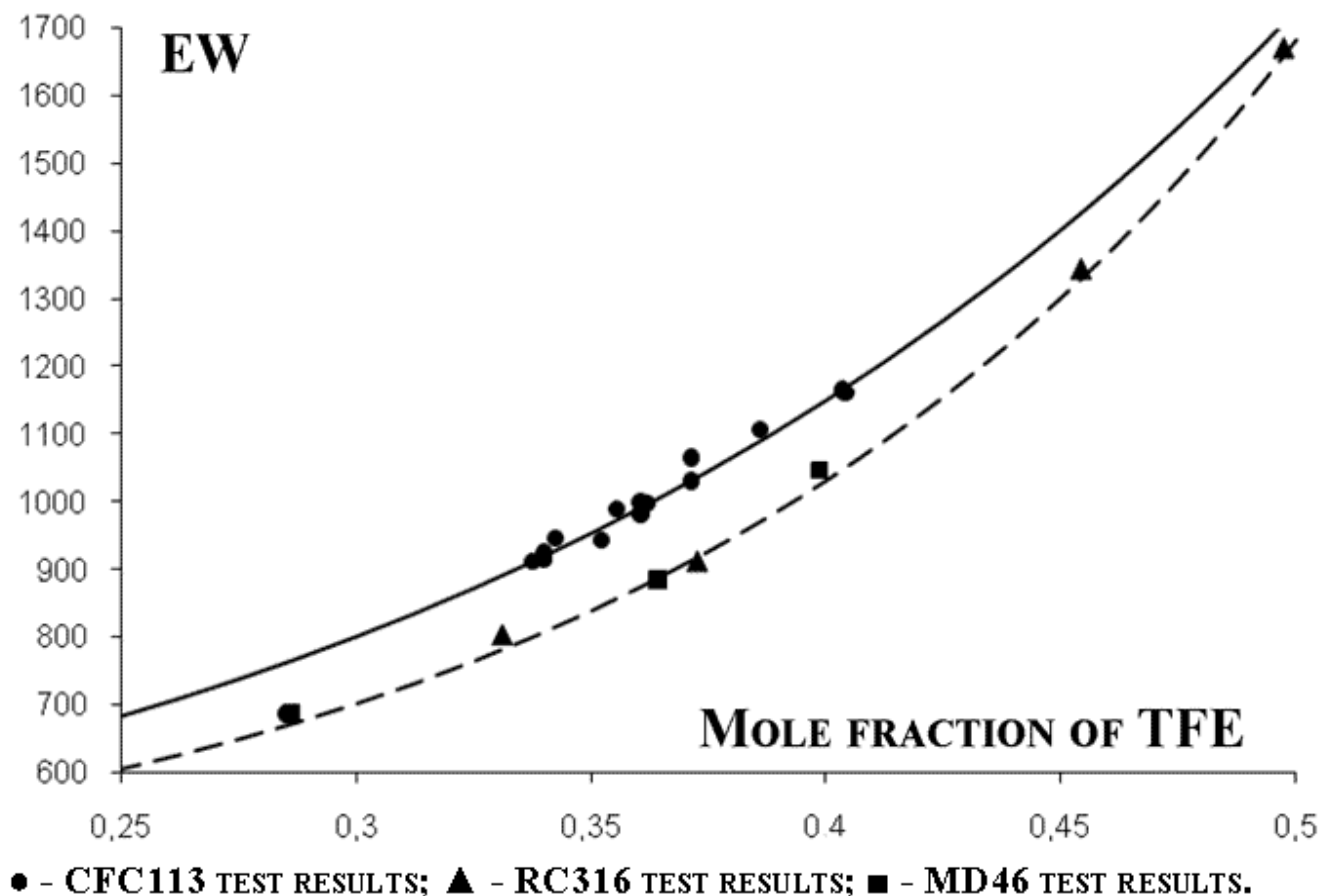
We further studied the solvent dependence of the co-polymer composition. In our calculations of TFE/PSVE co-polymer composition were applied the terminal link model developed by Frank R. Mayo and Frederick M. Lewis.

According to that model the copolymer composition follows the formula:

$$\frac{F_1}{F_2} = \frac{f_1}{f_2} \cdot \frac{r_1 \cdot f_1 + f_2}{r_2 \cdot f_2 + f_1}$$

Here F_1 and F_2 are mole shares of TFE and PSVE monomers in the copolymer; f_1 and f_2 those in the monomer blend; r_1 and r_2 are TFE and PSVE B co-polymerisation constants.

The graphically obtained results are shown in Figure 2.



EW- equivalent weightB

Figure 2. The co-polymer composition dependence on the TFE/PSVE mole ratio in the reaction blend.

We determined the constants at PSVE conversion values of 15-20%. For the polymerisation process conducted in CFC113 environment the constant values were $r_{TFE}= 23.3$; $r_{PSVE}=0.9$. In cases of MD46 and RC316 those values were $r_{TFE}= 73$; and $r_{PSVE}=5$, correspondingly.

Conclusions

1. The half-decay periods for DAP-C synthesized in MD-46 or RC-316 solvents are very close.
2. From our estimation of melt flow indices one may conclude that the molecular weights of copolymers prepared in MD46, RC316, and PSVE solvents exceed that of produced in CFC113.
3. The TFE/PSVEco-polymerisation constants calculated for MD46 and RC316 solvents differ considerably from those for CFC113, suggesting that CFC113 participates in the co-polymerisation process.
4. Any of considered solvents may perform as CFC113 substituent in this process. The obtained constant values allow high-accuracy prognostication of the co-polymer composition when the polymerization is conducted in RC316 or MD46.

References

1. Pat. 4116888 US, US CI 521/28. Process for producing fluorinated copolymer having ion-exchange groups.
2. Pat. 4349650 US, US CI 526/243. Polyfluoroalkoxy compounds, their preparation and copolymers therefrom.

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